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HYDROMECHANICS

COMPUTER PROGRAM DOCUMENTATION

STEAM CONDENSER DESIGN

AERODYNAMICS

by

STRUCTURAL MECHANICS



M. Botting

D. Kelly

APPLIED MATHEMATICS

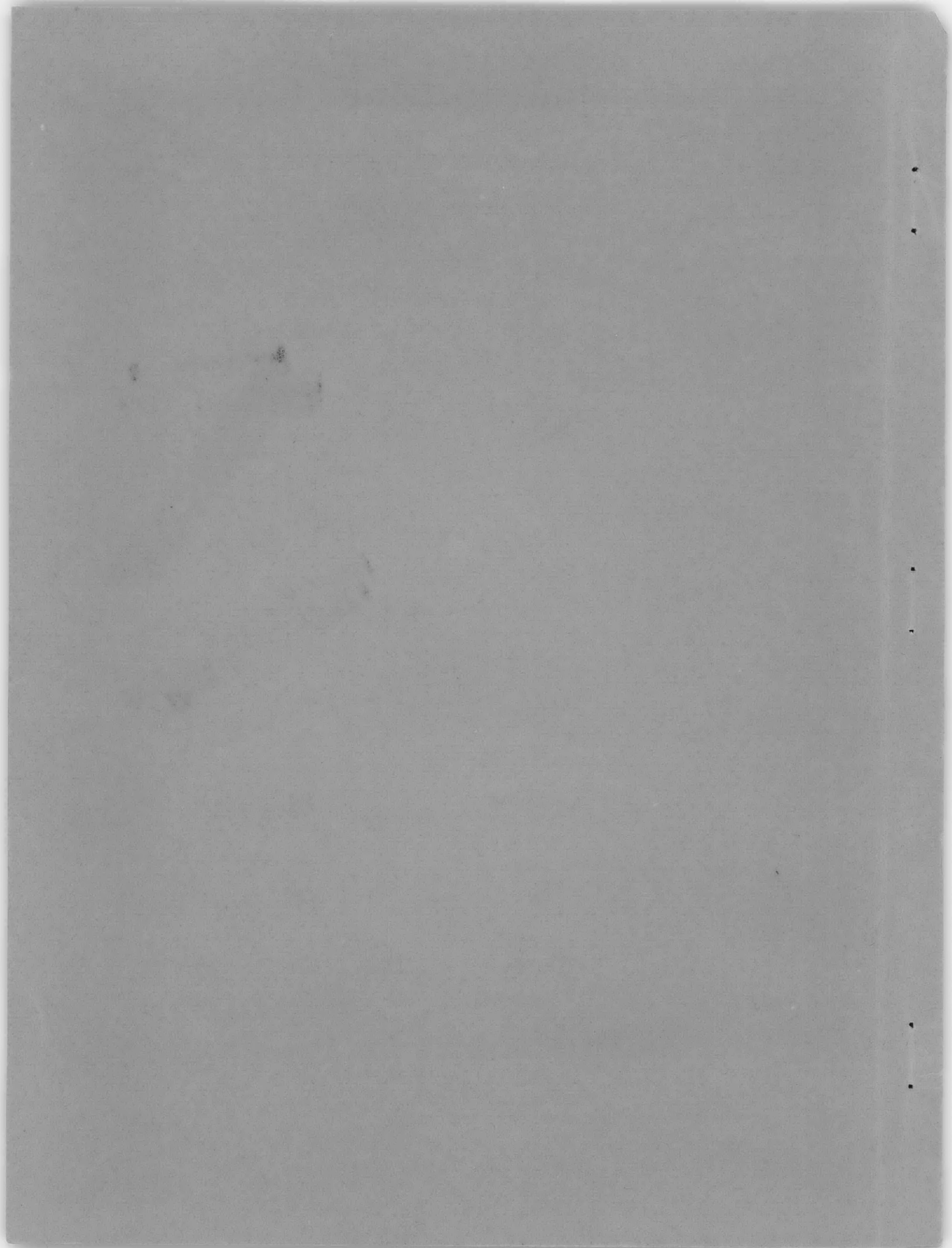
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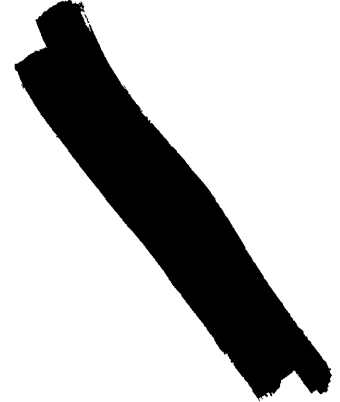
July 1966

Report 2255



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STEAM CONDENSER DESIGN

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Report 2255
SR003-0801
Task 10894

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ADMINISTRATIVE INFORMATION

This work was accomplished under project SR003-0801, Task 10894.

The Computer program and documentation herein has been approved by the Naval Ship Engineering Center for use in naval ship design.

The U. S. Government will incur no liability for loss arising from the use of the computer program described herein.

I. IDENTIFICATION DATA

A. Title - Steam Condenser Design

1. FORTRAN IV Deckname - COND
2. Revision - A - Original Issue

B. Abstract - This program calculates all the necessary information required for the selection of main or auxiliary steam condensers to either preliminary or contract design requirements.

For preliminary design a graph is also provided which relates condenser overall length with tube sheet diameter for a specified set of design conditions. For contract design a graph relating condenser absolute pressure and increments of heat rejection at integer circulating water velocities is also provided for analysis of part load performance.

C. Input/Calculated Items/Output

1. Input

| <u>Term</u> | <u>Standard Symbol</u> |
|--|------------------------|
| Tube Material | XMA1TU |
| Tube Gage | GA1TU |
| Tube Outside Diameter (inches) | D5TU |
| Number of Passes | XN2PS |
| Cleanliness Factor | F2TCLN |
| Number of Tube Sheets per end | XN2TSE |
| Ineffective Tube Length per end (inches) | XL1TUI |

| <u>Term</u> | <u>Standard Symbol</u> |
|--|------------------------|
| Tube Hole Space Factor | F2TUHO |
| Steam Flow to Condenser (lb/hr) | R9SF5 |
| Heat Rejected per pound of Steam (BTU/lb) | HTISR |
| Design Back Pressure (inches-hg) | P2BDES |
| Injection Water Temperature (^o F.) | TEIINJ |
| Overall Condenser Length Desired (ft) | XLITT |
| Desired Diameter of Tube Sheet (ft) | D5COND |
| Circulating Water Velocity in Tubes (ft/sec) | VIWTU |
| Ordered Tube Length Shortest | XLITUO |
| Ordered Tube Length Longest | QLITUO |

2. Internal Values

| <u>Term</u> | <u>Standard Symbol</u> |
|---------------------------------|------------------------|
| Tube Wall Thickness | TH1TU |
| Basic Heat Transfer Coefficient | C1HEAT |
| Tube Constant | C9TU |
| Material and Gage Factor | F2MG |
| Temperature Correction Factor | F2TEC |
| GPM/1 FPS/Tube | F1V6TU |

3. Output

| <u>Term</u> | <u>Standard Symbol</u> |
|------------------------------|------------------------|
| Temperature Saturated Liquid | TEISAT |
| Ordered Tube Length | XLITUO |
| Tube Surface Area | S2TU |

| <u>Term</u> | <u>Standard Symbol</u> |
|------------------------------------|------------------------|
| Effective Tube Length | XL1TUE |
| Number of Tubes | XN2TUT |
| Tube Sheet Diameter | D5TUSH |
| Tube Sheet Area | ALTUSH |
| Overall Condenser Length | XL1CON |
| Circulating Water Required (GPM) | R9SW2 |
| Circulating Water Outlet Temp. | TE1O |
| Terminal Temperature Diff. | TE1TD |
| Circulating Water Temperature Rise | TE1R |

D. Author/Date

Maxine Botting Denis Kelly December 1965

E. Organization

Computer-Aided Ship Design Division, Code 850, David Taylor
Model Basin.

F. Computer/Source Language

IBM 7090 FORTRAN IV CARD INPUT

G. Reference to Documentation

DTMB Report 2255 of July 1966

H. Security Classification

Unclassified

I. Estimated Running Time

1 1/2 minutes.

II. PURPOSE AND METHOD

A. Description of Method

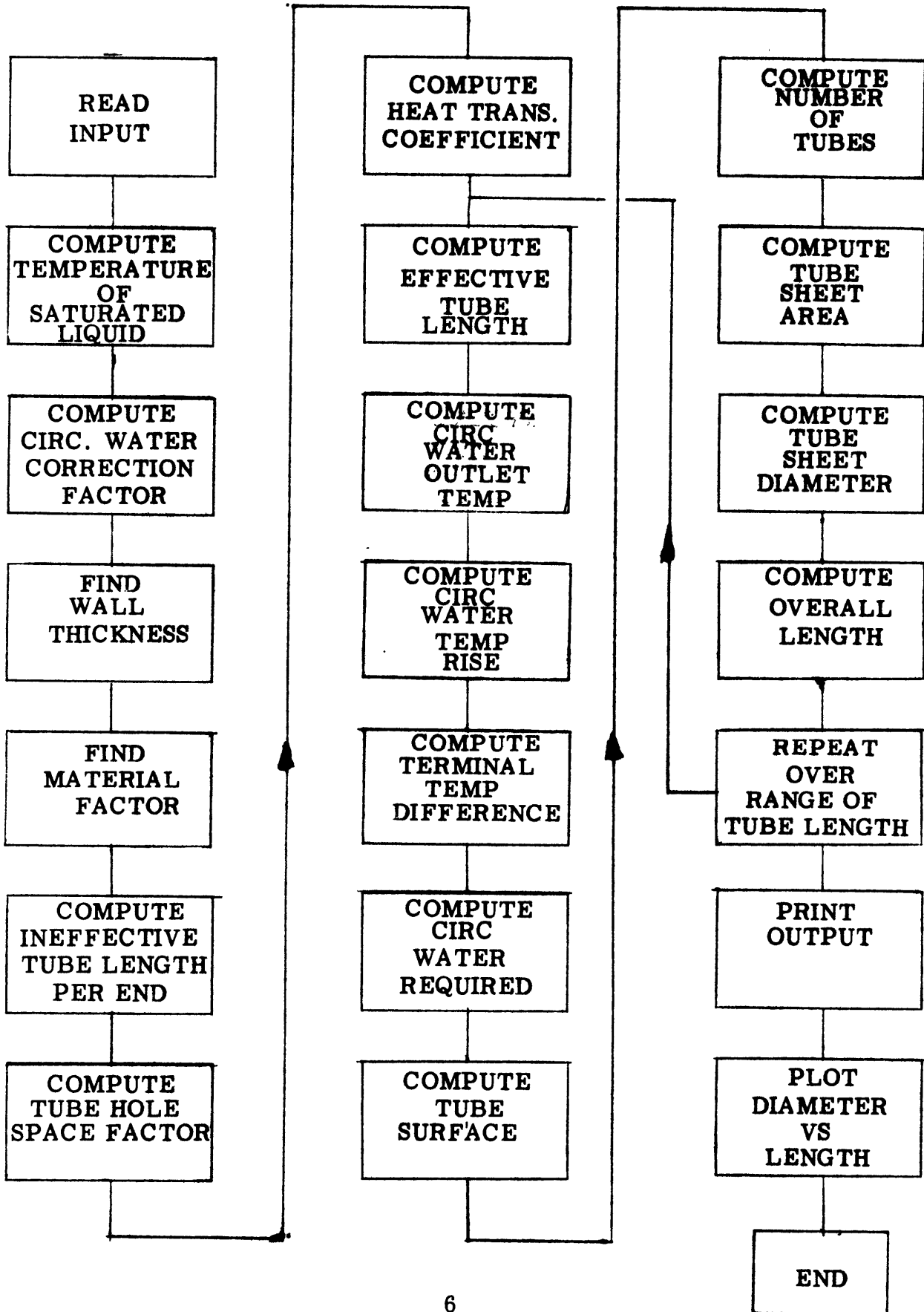
The purpose of this program is to develop the required design data necessary for the selection of a steam condenser in accordance with the ordering data specified in military specification MIL-C-15430G. Since any condenser design is a balance of tube surface, tube length and cooling water quantity, it is the space allowed for the condenser that actually is the deciding factor in the design. If the limiting dimensions are known the contract design mode is employed and the design is calculated based on these specific dimensions. If exact limiting dimensions are not known, a range of tube lengths can be specified, the preliminary design mode employed, and a number of satisfactory designs reviewed.

The theory and formulations of the design process are shown in design data sheet DDS4601-1 of 15 October 1953.

The temperature of a saturated liquid as a function of pressure and pressure as a function of temperature are obtained by formulations developed by Westinghouse Corporation based on Keenan and Keyes values.

A simple descriptive flow chart is as follows:

PRELIMINARY DESIGN MODE



Contract Design Mode

In the contract design mode an estimated ordered tube length is computed based on the overall condenser length used as input. The above calculations are then performed and a calculated overall length developed. This value is compared with the desired overall length. If larger the ordered tube length is incremented six inches smaller and the calculations repeated. When the calculated length is equal or smaller the program then checks the tube sheet diameter. If the calculated value is too large the program stops. If it is satisfactory a plot of heat load versus absolute pressure is developed for various circulating water velocities from input value down to 3 feet/sec.

B. Assumptions

Tube materials and gage factors for 12 and 13 BWG are extrapolated from HEI standards for steam surface condensers which include only 14-18 BWG.

C. References

1. Design Data Sheet DDS4601-1 of 15 October 1953 - Steam Condensers.
2. Military Specification MIL-C-15430G Condensers, Steam Surface, Naval Shipboard.
3. Share Programs C3-WH58-PA-3137 (Westinghouse Corporation Properties of Steam).

III. RESTRICTIONS

A. Non-standard subroutines not included in the program are the North American S-C 4020 subroutine package.

B. A tape is required on B-9 to go to the S-C 4020.

C. Non-standard hardware is the S-C 4020.

D. Maximum Array Size

In the preliminary design mode there is a limit of 10 tube lengths starting with the shortest and increasing at six inch intervals.

IV. NON-STANDARD OPERATING INSTRUCTIONS

- A. There are no special operating instructions.
- B. There are no restart instructions.
- C. There are no on line error corrections.
- D. Validation Checks

The program has been checked and found to be accurate against the sample problems contained in design data sheet DDS4601-1 of 15 October 1953.

V. DATA PREPARATION

A. Card Input Description

All input except the first card is a 12 column fields. The specified columns are where a typical value would be. Decimal points are necessary and all values should be right adjusted.

For limitations on input see VI-C- SPECIAL DIAGNOSTICS.

| <u>CARD</u> | <u>DATA</u> | <u>TYPICAL FIELD</u> | <u>INPUT PARAMETERS</u> | <u>COLUMNS</u> |
|-------------|--|--------------------------|---|----------------|
| First | Title for output (Must be centered in field to be cen- tered on output) | | | 1 - 72 |
| Second | (Tube Material) | X. | 1. (70 - 30 CU-NI) 2. (90 - 10 CU-NI) | 11 - 12 |
| Second | (Tube Gage) | XX. | 12 to 18 | 22 - 24 |
| Second | (Tube Diameter) | .XXX | .625 .750 .875 | 33 - 36 |
| Second | (Cleanliness Factor) | .XX | .85 (Typical Value) | 46 - 48 |
| Second | (No. of Tube Sheets/ end) | X. | 1. or 2. | 59 - 60 |
| Second | (Ineffective Tube Length per end) | X. | If 0 program will calculate this value | 71 - 72 |
| Third | (Tube Hole Space Factor) | X.XX | If 0 program will calculate this value | 9 - 12 |
| Third | (No. of passes) | X. | | 23 - 24 |
| Third | (Steam to Condenser) | XXXXXXXX. | | 30 - 36 |
| Third | (Heat Rejected | XXX. | | 45 - 48 |
| Third | (Design Back Pressure) | XX.X | | 57 - 60 |

| <u>CARD</u> | <u>DATA</u> | <u>TYPICAL FIELD</u> | <u>INPUT PARAMETERS</u> | <u>COLUMN</u> |
|-------------|---------------------------------------|--------------------------|--|---------------|
| Third | (Circ. Water Velocity) | XX. | | 70 - 72 |
| Fourth | (Injection water temperature) | XX. | | 10 - 12 |
| Fourth | (Desired overall condenser length) | XX. X | If 0 will execute pre- liminary design If a value will exe- cute contract design | 21 - 24 |
| Fourth | (Desired diameter of tube sheet) | XX. X | | 33 - 36 |
| Fourth | (Shortest ordered tube length) | XX. X | } Must be 10 values or less at 6 inch intervals between shortest and longest ordered tube length | 57 - 60 |
| Fourth | (Longest ordered tube length) | XX. X | | |

C. Output Form Description

The input data is printed as the first output in each mode. In the preliminary design mode the desired overall condenser length and tube sheet diameter values are zero. The calculated output is self-explanatory for each mode. Graphic output for the preliminary mode shows the relationship between circular tube sheet diameter and overall condenser length for a given set of design conditions. Graphic output for the contract design mode shows condenser part load performance with the condenser absolute pressure and heat rejection load (up to 110% of full power) shown at various circulating water velocities.

TEST CASE 1

CONDENSER DESIGN PROGRAM

INPUT VALUES

| | |
|---|---------|
| TUBE MATERIAL | 90-10 |
| TUBE GAGE | 18. |
| TUBE DIAMETER (IN) | 0.6250 |
| CLEANLINESS FACTOR | 0.8500 |
| NUMBER OF TUBE SHEETS PER END | 1. |
| INEFFECTIVE TUBE LENGTH PER END (IN) | 0. |
| TUBE HOLE SPACE FACTOR | 0. |
| NUMBER OF PASSES | 1. |
| STEAM TO CONDENSER (LB/HR) | 217000. |
| HEAT REJECTED PER POUND OF STEAM (BTU/LB) | 936.00 |
| DESIGN BACK PRESSURE (IN HG) | 5.00 |
| CIRC WATER VELOCITY IN TUBES (FT/SEC) | 9.00 |
| INJECTION WATER TEMPERATURE (DEG F) | 75.00 |
| DESIRED OVERALL CONDENSER LENGTH (FT) | 0. |
| DESIRED DIAMETER OF TUBE SHEET (FT) | 0. |
| ORDERED TUBE LENGTH SHORTEST (FT) | 9.00 |
| ORDERED TUBE LENGTH LONGEST (FT) | 12.00 |

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V. D-1 SAMPLE OUTPUT
PRELIMINARY DESIGN MODE

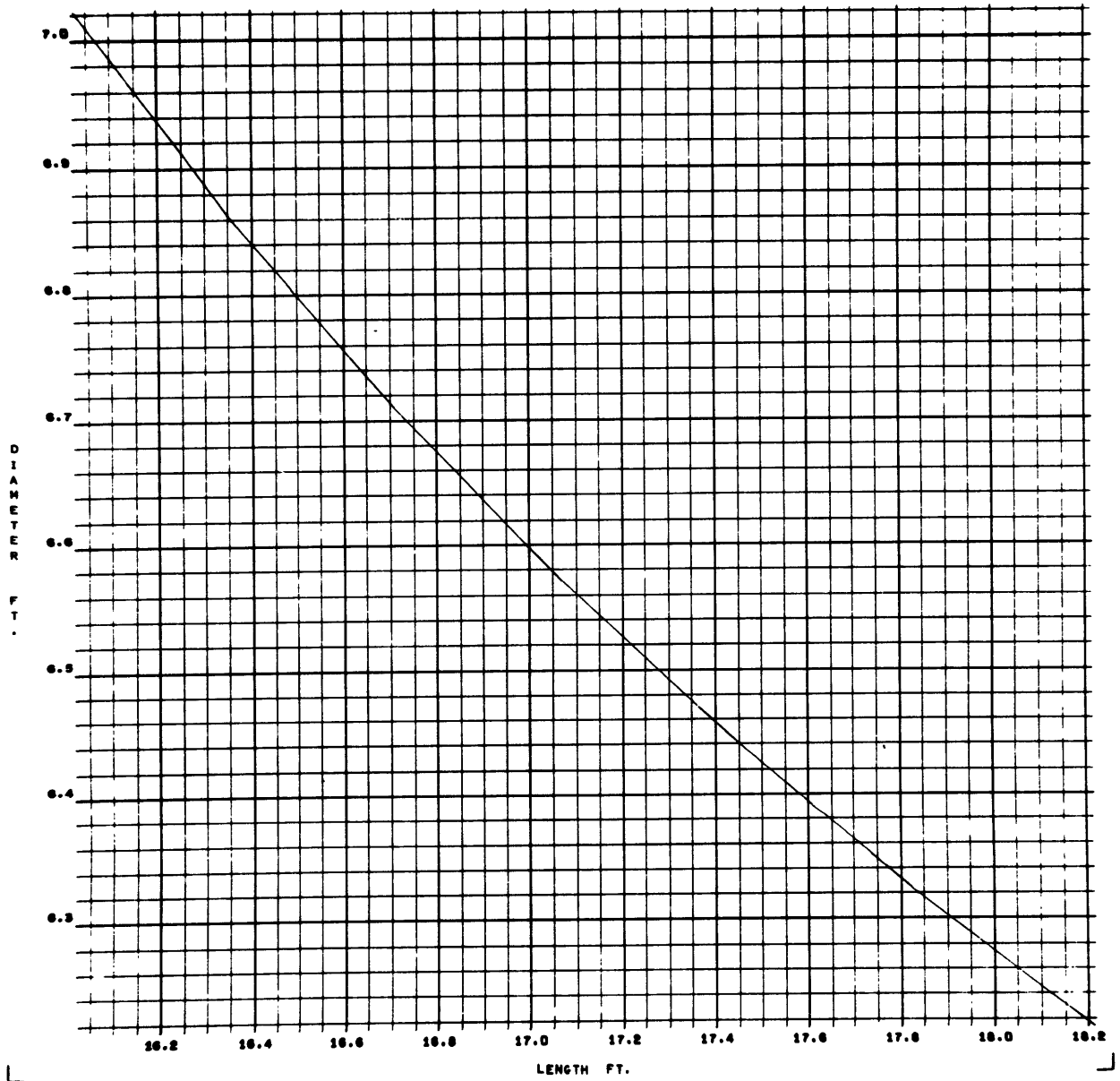
CUTPUT VALUES

| | | | | | | | | |
|----|--------------------------------------|--------|--------|----------|--------|--------|--------|--------|
| | TEMPERATURE SATURATED LIQUID (DEG F) | | | 133.7590 | | | | |
| | ORDERED TUBE LENGTH (FT) | 9.00 | 9.50 | 10.00 | 10.50 | 11.00 | 11.50 | 12.00 |
| | TUBE SURFACE AREA (SQ FT) | 6299. | 6350. | 6401. | 6452. | 6504. | 6556. | 6608. |
| | EFFECTIVE TUBE LENGTH (FT) | 8.82 | 9.32 | 9.82 | 10.32 | 10.82 | 11.32 | 11.82 |
| | NUMBER OF TUBES | 4364. | 4163. | 3983. | 3820. | 3673. | 3539. | 3416. |
| | TUBE SHEET DIAMETER (FT) | 7.02 | 6.86 | 6.71 | 6.57 | 6.44 | 6.32 | 6.21 |
| | TUBE SHEET AREA (SQ FT) | 38.74 | 36.96 | 35.36 | 33.91 | 32.61 | 31.42 | 30.32 |
| | OVERALL CONDENSER LENGTH (FT) | 16.02 | 16.36 | 16.71 | 17.07 | 17.44 | 17.82 | 18.21 |
| 16 | CIRCULATING WATER REQD (GPM) | 26697. | 25469. | 24368. | 23374. | 22473. | 21652. | 20902. |
| | CIRC WATER OUTLET TEMP (DEG F) | 90.22 | 90.95 | 91.67 | 92.38 | 93.08 | 93.76 | 94.43 |
| | TERMINAL TEMP DIFF (DEG F) | 43.54 | 42.81 | 42.09 | 41.38 | 40.68 | 40.00 | 39.32 |
| | CIRC WATER TEMP RISE (DEG F) | 15.22 | 15.95 | 16.67 | 17.38 | 18.08 | 18.76 | 19.43 |

V. D-1 SAMPLE OUTPUT
PRELIMINARY DESIGN MODE

V. D-1 SAMPLE OUTPUT
PRELIMINARY DESIGN MODE

TEST CASE 1 CONDENSER DESIGN PROGRAM



INPUT VALUES

| | |
|---|---------|
| TUBE MATERIAL | 90-10 |
| TUBE GAGE | 18. |
| TUBE DIAMETER (IN) | 0.6250 |
| CLEANLINESS FACTOR | 0.8500 |
| NUMBER OF TUBE SHEETS PER END | 1. |
| INEFFECTIVE TUBE LENGTH PER END (IN) | 0. |
| TUBE HOLE SPACE FACTOR | 0. |
| NUMBER OF PASSES | 1. |
| STEAM TO CONDENSER (LB/HR) | 217000. |
| HEAT REJECTED PER POUND OF STEAM (BTU/LB) | 936.00 |
| DESIGN BACK PRESSURE (IN HG) | 5.00 |
| CIRC WATER VELOCITY IN TUBES (FT/SEC) | 9.00 |
| INJECTION WATER TEMPERATURE (DEG F) | 75.00 |
| DESIRED OVERALL CONDENSER LENGTH (FT) | 18.00 |
| DESIRED DIAMETER OF TUBE SHEET (FT) | 10.00 |
| ORDERED TUBE LENGTH SHORTEST (FT) | 0. |
| ORDERED TUBE LENGTH LONGEST (FT) | 0. |

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V. D-2 SAMPLE OUTPUT
CONTRACT DESIGN MODE

OUTPUT VALUES

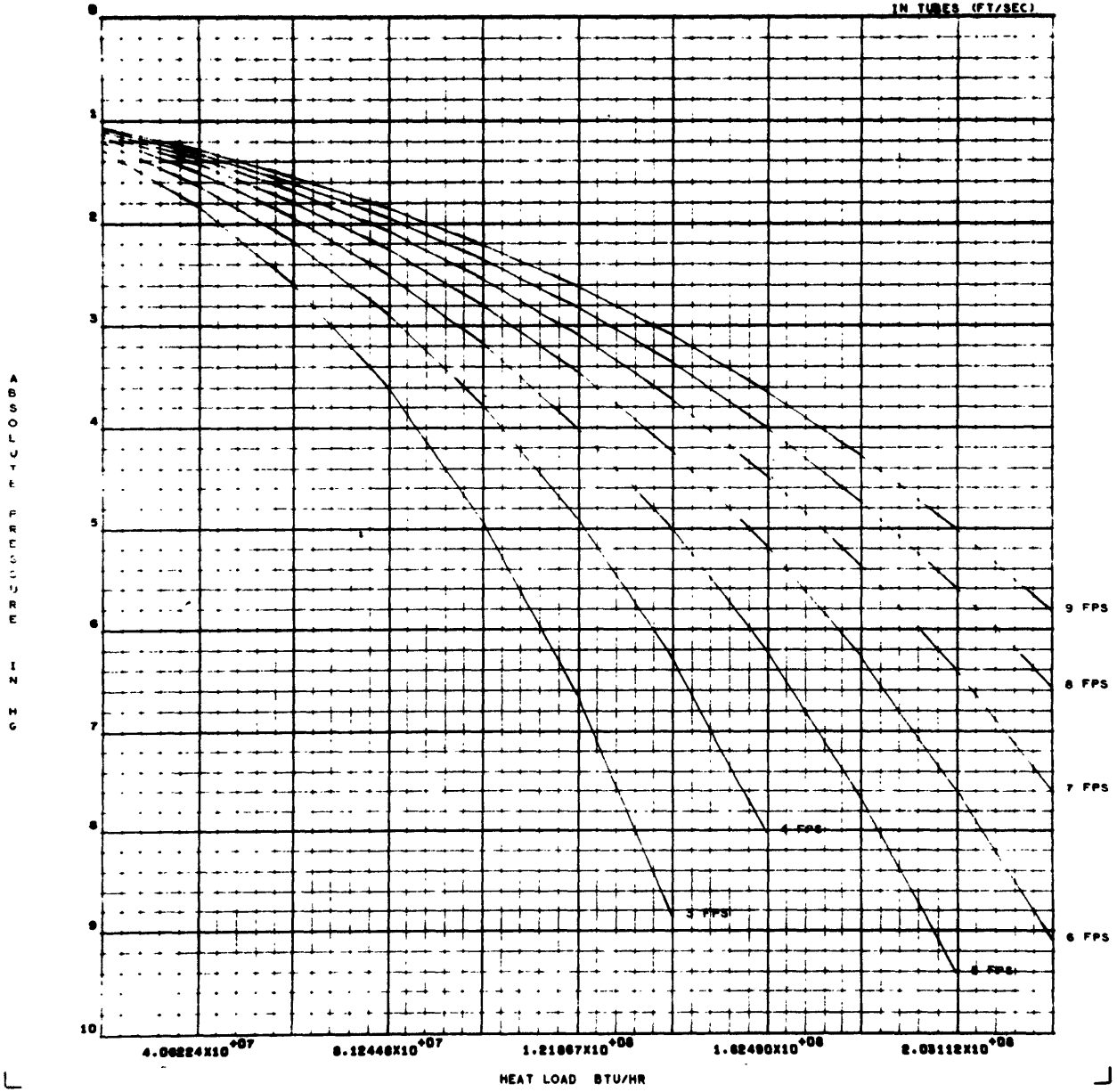
| | |
|--------------------------------------|----------|
| TEMPERATURE SATURATED LIQUID (DEG F) | 133.7590 |
| ORDERED TUBE LENGTH (FT) | 11.50 |
| TUBE SURFACE AREA (SQ FT) | 6556. |
| EFFECTIVE TUBE LENGTH (FT) | 11.32 |
| NUMBER OF TUBES | 3539. |
| TUBE SHEET DIAMETER (FT) | 6.32 |
| TUBE SHEET AREA (SQ FT) | 31.42 |
| OVERALL CONDENSER LENGTH (FT) | 17.82 |
| 19 CIRCULATING WATER REQD (GPM) | 21652. |
| CIRC WATER OUTLET TEMP (DEG F) | 93.76 |
| TERMINAL TEMP DIFF (DEG F) | 40.00 |
| CIRC WATER TEMP RISE (DEG F) | 18.76 |

V. D-2 SAMPLE OUTPUT
CONTRACT DESIGN MODE

V. D-2 SAMPLE OUTPUT CONTRACT DESIGN MODE

TEST CASE 2 CONDENSER DESIGN PROGRAM

CIRC WATER VELOCITY
IN TUBES (FT/SEC)



E. Symbol List

See list in I. C.

F. Data Tables Used by Program

1. Factors used in determining saturated liquid temperature:

Reference (3)

| | |
|-------|------------------------|
| (QAA) | $A_0 = 35.15789$ |
| | $A_1 = 24.592588$ |
| | $A_2 = 2.1182069$ |
| | $A_3 = -.3414474$ |
| | $A_4 = .15741642$ |
| | $A_5 = -.031329585$ |
| | $A_6 = .0038658282$ |
| | $A_7 = -.00024901784$ |
| | $A_8 = .0000068401559$ |

2. Circulating Water Temperature Correction Factors:

Reference (1)

| | |
|-------|-----------------------------|
| (QCF) | $30^{\circ}\text{F} = .65$ |
| | $35^{\circ}\text{F} = .70$ |
| | $40^{\circ}\text{F} = .75$ |
| | $45^{\circ}\text{F} = .798$ |
| | $50^{\circ}\text{F} = .843$ |
| | $55^{\circ}\text{F} = .886$ |
| | $60^{\circ}\text{F} = .926$ |

| | |
|-------|---------------------------|
| (QCF) | 65 ^o F = .963 |
| | 70 ^o F = 1.0 |
| | 75 ^o F = 1.025 |
| | 80 ^o F = 1.045 |
| | 85 ^o F = 1.061 |
| | 90 ^o F = 1.076 |
| | 95 ^o F = 1.09 |
| | 100 ^o F = 1.1 |

3. Wall Thickness Factors: Reference (1) and page 6, II B

| | |
|-------|---------------|
| (QTH) | BWG 12 - .109 |
| | 13 - .095 |
| | 14 - .083 |
| | 15 - .072 |
| | 16 - .065 |
| | 17 - .058 |
| | 18 - .049 |

4. Material and Gage Factors: Reference (1) and page 6, II B

| (QCU) | <u>CU-NI 70-30</u> | <u>CU-NI 90-10</u> | <u>BWG</u> |
|-------|--------------------|--------------------|------------|
| | .46 | .55 | 12 |
| | .55 | .64 | 13 |
| | .64 | .72 | 14 |
| | .71 | .79 | 15 |

| <u>CU-NI 70-30</u> | <u>CU-NI 90-10</u> | <u>BWG</u> |
|--------------------|--------------------|------------|
| .76 | .84 | 16 |
| .80 | .87 | 17 |
| .83 | .90 | 18 |

5. Factors Used in Determining Saturation Pressure of a Saturated

Liquid: Reference (3)

(QPFT)

A = 3.2437814

B = .00586826

C = 1.1702379E-8

D = .0021878462

E = 0.0

A = 3.346313

B = .0414113

C = 7.515484E-9

D = .013794481

E = 6.56444E-11

VI CODING INFORMATION

A. Flow Charts

I

COMMON XMA1TU,GA1TU,D5TU,F2TCLN,XN2TSE,XL1TUI

COMMON F2TUHO,XN2PS,R9SF5,HT1SR,P2BDES,V1WTU

COMMON TE1INJ,XL1TT,D5COND,XL1TUO,QL1TUO

COMMON S2TU,XL1TUE,XN2TUT,D5TUSH,A1TUSH,XL1CON

COMMON R9SW2,TE10,TE1TD,TE1R,W2COND,VL1HW

DIMENSION QTITLE(12)

DIMENSION QAA(9),QCU(7,2),QCF(15),QTH(7)

DIMENSION QPFT(5,2),QMA(2)

DIMENSION QP1(11),QP2(11),QP3(10),QP4(10),QP5(10),QP6(10),QP7(10),QP8(10),QP9(10),QP10(10),QP11(10)

SEE DATA STATEMENT

QAA

SEE DATA STATEMENT

QCU

SEE DATA STATEMENT

QCF

SEE DATA STATEMENT

QTH

SEE DATA STATEMENT

QPFT

DATA QAA/35.15789,24.592588,2.1182069,-.3414474,.15741642,
.3132958E-1,.38658282E-2,-.24901784E-3,.68401559E-5/

DATA QCU/.46,.55,.64,.71,.76,.80,.83,.55,.64,.72,.79,.84,
.87,.90/

DATA QCF/.65,.7,.75,.798,.843,.886,.926,.963,1.,1.025,
1.045,1.061,1.076,1.09,1.1/

DATA QTH/.109,.095,.083,.072,.065,.058,.049/

DATA QPFT/3.2437814,.00586826,1.1702379E-8,.0021878462,0.,
3.346313,.0414113,7.515484E-9,.013794481,6.56444E-11/

DATA QMA/6H 70-30,6H 90-10/

1 FORMAT (12A6)

2 FORMAT (1H1,/,24X,12A6,/, ,13H0INPUT VALUES,//)

3 FORMAT (6E12.6)

5 FORMAT(14HOTUBE MATERIAL,40X,A6/10H TUBE GAGE,30X,F20.0/
20H TUBE DIAMETER (IN),20X,F20.4)

6 FORMAT (19H CLEANLINESS FACTOR,21X,F20.4/30H NUMBER OF TUBE
SHEETS PER END,10X,F20.0/38H INEFFECTIVE TUBE LENGTH PER
END (IN),F22.4)

7 FORMAT(23H TUBE HOLE SPACE FACTOR,17X,F20.4,/17H NUMBER OF
PASSES,23X,F20.0,/28H STEAM TO CONDENSER (LB/HR),F32.0)

8 FORMAT(43H HEAT REJECTED PER POUND OF STEAM (BTU/LB),F17.2,/30H
DESIGN BACK PRESSURE (IN HG),F30.2,/39H CIRC WATER
VELOCITY IN TUBES (FT/SEC,F21.2)

9 FORMAT (37H INJECTION WATER TEMPERATURE (DEG F),F23.2,/39H
DESIRED OVERALL CONDENSER LENGTH (FT),F21.2,/37H DESIRED
DIAMETER OF TUBE SHEET (FT),F23.2)

10 FORMAT (36H ORDERED TUBE LENGTH SHORTEST (FT),F24.2,/35H
ORDERED TUBE LENGTH LONGEST (FT),F25.2)

15 FORMAT (6E20.8)

20 FORMAT (22H0INPUT VALUE P2BDES IS,E15.8,5X,28HSHOULD BE BETWE
AND 450)

21 FORMAT (22H0INPUT VALUE TE1INJ IS,E15.8,5X,28HSHOULD BE BETWE
AND 100)

22 FORMAT (21H0INPUT VALUE GAITU IS,E15.8,5X,27HSHOULD BE BETWEE
AND 18)

23 FORMAT (22H0INPUT VALUE XMA1TU IS,E15.8,5X,16HSHOULD BE 1 OR

24 FORMAT (19H0XL1TUI IS NEGATIVE,E15.8)

25 FORMAT (22H0INPUT VALUE XN2TSE IS,E15.8,5X,16HSHOULD BE 1 OR

26 FORMAT (19H0F2TUHO IS NEGATIVE,E15.8)

27 FORMAT (1H0,30X,36HTERMINAL TEMP DIFF LESS THAN 5 DEG F)

28 FORMAT (36H0DIAMETER OF TUBE SHEET IS TOO LARGE)

39 FORMAT (14H1OUTPUT VALUES,/,38H0TEMPERATURE SATURATED
LIQUID (DEG F),F22.4)

40 FORMAT (26H0ORDERED TUBE LENGTH (FT),4X,10F9.2)

41 FORMAT (27H0TUBE SURFACE AREA (SQ FT),3X,10F9.0)

42 FORMAT (28H0EFFECTIVE TUBE LENGTH (FT),2X,10F9.2)

43 FORMAT (16H0NUMBER OF TUBES,14X,10F9.0)

44 FORMAT (26H0TUBE SHEET DIAMETER (FT),4X,10F9.2)

45 FORMAT (25H0TUBE SHEET AREA (SQ FT),5X,10F9.2)

46 FORMAT (31H0OVERALL CONDENSER LENGTH (FT),F8.2,9F9.2)

```

47     FORMAT (20H0CIRCULATING WATER REQD (GPM),10F9.0)
48     FORMAT (22H0CIRC WATER OUTLET TEMP (DEG F),F7.2,9F9.2)
49     FORMAT (28H0TERMINAL TEMP DIFF (DEG F),2X,10F9.2)
50     FORMAT (30H0CIRC WATER TEMP RISE (DEG F),10F9.2)

      CALL CAMRAV (35)

```

READ INPUT

SEE NEXT STATEMENT QTITLE

```

***READ(5,1)QTITLE
***READ(5,3)XMA1TU,GA1TU,D5TU,F2TCLN,XN2TSE,XL1TUI
***READ(5,3)F2TUHO,XN2PS,R9SF5,HT1SR,P2BDES,V1WTU

```

SEE NEXT STATEMENT QL1TUO

```

***READ(5,3)TE1INJ,XL1TT,D5COND,XL1TUO,QL1TUO

```

PRINT INPUT

```

***WRITE(6,2)QTITLE
      I=XMA1TU
***WRITE(6,5)QMA(I),GA1TU,D5TU
***WRITE(6,6)F2TCLN,XN2TSE,XL1TUI
***WRITE(6,7)F2TUHO,XN2PS,R9SF5
***WRITE(6,8)HT1SR,P2BDES,V1WTU
***WRITE(6,9)TE1INJ,XL1TT,D5COND
***WRITE(6,10)XL1TUO,QL1TUO

```

SEE NEXT STATEMENT MPTS

```

      I
      I MPTS =0
      I P2BDES =P2BDES*.49115
      I
      I

```

I

COMPUTE TEMPERATURE OF SATURATED LIQUID

```

      I
      I
      . * * .
    . * * IF * .
  * * (P2BDES-.2) *
I * . * * I
I * . * * I
I * . * * I
- I      0 I      + I
-----
I 105 I      I 106 I      I 106 I
-- --

```

105 ***WRITE(6,20)P2BDES

STOP

```

      I
      I
      . * * .
    . * * IF * .
  * * (P2BDES-450.) *
I * . * * I
I * . * * I
I * . * * I
- I      0 I      + I
-----
I 109 I      I 105 I      I 105 I
-- --

```

```

      I
109      I TE1SAT =QAA(1)      I

```

```

      I
      SEE NEXT STATEMENT      QT1

```

```

      I
      I QT1 =1.      I

```

```

      I
      SEE NFXT STATEMENT      QT2

```

```

      I
      I QT2 =ALOG(10.*P2BDES)      I

```

```

          I
          I
        + DO
    ++++++ 110
    +      + K=2,9
    +      +
    +      I
    +      I
    +      I
    +      I
    +      I
    +      I
    +      I
    +      I
110 ++++++I TE1SAT =TE1SAT+QAA(K)*QT1

```

***WRITE (6,39)TE1SAT

COMPUTE CIRC WATER CORRECTION FACTOR

```

          I
          I
        . * * .
    . * * IF * .
    * (TE1INJ-30.) *
    I * .
    I * .
    I * .
    - I 0 I + I
---*+
I 115 I I 116 I I 116 I
-- +

```

115 ***WRITE(6,21)TE1INJ

STOP

```

          I
          I
        . * * .
    . * * IF * .
    * (TE1INJ-100.) *
    I * .
    I * .
    I * .
    - I 0 I + I
---*+
I 120 I I 120 I I 115 I
-- -

```

I


```

120      I K      =TE1INJ/5.-5.          I
        I QT1    =(K+5)*5              I
        I F2TEC=QCF(K)+(QCF(K+1)-QCF(K)) I
        I          *(TE1INJ-QT1)*.2    I
        I

```

FIND WALL THICKNESS

```

        I
        I
        . * . * .
        * * IF * *
        * (GA1TU-12.) *
        I * . * * I
        I * . * * I
        I * . * * I
        - I      0 I      + I
        -----
        I 121 I      I 122 I      I 122 I
        ---*--

```

```

121      ***WRITE(6,22)GA1TU

```

STOP

```

122      I
        I
        . * . * .
        * * IF * *
        * (GA1TU-18.) *
        I * . * * I
        I * . * * I
        I * . * * I
        - I      0 I      + I
        -----
        I 125 I      I 125 I      I 121 I
        ---

```

```

        I
125      I K      =GA1TU-11.          I
        I TH1TU=QTH(K)              I
        I

```

FIND MATERIAL FACTOR

```

      I
      I
      . * * .
    . * * IF * .
  * (XMA1TU-1.) *
  I * . * . * I
  I * . * . * I
  I * . * . * I
- I      0 I      + I
-----
I 126 I      I 128 I      I 127 I
---+-

```

126 ***WRITE(6,23)XMA1TU

STOP

```

      I
      I
      . * * .
    . * * IF * .
  * (XMA1TU-2.) *
  I * . * . * I
  I * . * . * I
  I * . * . * I
- I      0 I      + I
---*-
I 126 I      I 128 I      I 126 I
---*-

```

```

      I
      I L      =XMA1TU      I
      I F2MG =QCU(K,L)      I
      I

```

COMPUTE INEFFECTIVE TUBE LENGTH PER END

```

      I
      I
      . * * .
    . * * IF * .
  * (XL1TUI) *
  I * . * . * I
  I * . * . * I
  I * . * . * I
- I      0 I      + I
-----
I 140 I      I 145 I      I 150 I
-----

```

140 ***WRITE(6,24)XL1TUI

```

          STOP
                I
                I
145      . * * .
        . * * IF * .
      * (XN2TSE-1.) *
    I * . * * I
    I * . * * I
    I * . * * I
  - I      0 I      + I
  ----
I 146 I      I 147 I      I 148 I
  ---*--

```

```

146      ***WRITE(6,25)XN2TSE

```

```

          STOP
                I
147      I XL1TUI =1.0625
                I
                I
          --
          I 150 I
          --

```

```

                I
                I
148      . * * .
        . * * IF * .
      * (XN2TSE-2.) *
    I * . * * I
    I * . * * I
    I * . * * I
  - I      0 I      + I
  ----
I 146 I      I 149 I      I 146 I
  ---*--

```

```

                I
149      I XL1TUI =6.25
                I

```

COMPUTE TUBE HOLE SPACE FACTOR

```

150      . * * .
      . * * IF * .
      * (F2TUHO) *
      I * . * * I
      I * . * * I
      - I      0 I      + I
      ----
      I 151 I      I 152 I      I 160 I
      --*+

```

```

151      ***WRITE(6,26)F2TUHO

```

```

      STOP

```

```

152      I
      I
      . * * .
      . * * IF * .
      * (P2BDES-1.25) *
      I * . * * I
      I * . * * I
      I * . * * I
      - I      0 I      + I
      ---+--
      I 153 I      I 153 I      I 154 I
      -- -

```

```

153      I
      I F2TUHO =.22      I
      I
      I
      --
      I 160 I
      --

```

```

154      I
      I F2TUHO =.24      I
      I

```

COMPUTE HEAT TRANSFER COEFFICIENT

```

160      I
      I
      . * * .
      . * * IF * .
      * (D5TU-.875) *
      I * . * * I

```

32

```

      I      * .      . *      I
      I      * . *      I
    - I      0 I      + I
  ---*---
I 162 I      I 161 I      I 161 I
  ---

```

```

      I
161      I C1HEAT =263.      I

```

```

      I
      I
      --
      I 180 I
      --

```

```

      I
162      I C1HEAT =270.      I

```

```

      I

```

COMPUTE GPM / TUBE / 1 FPS VELOCITY

```

      I
180      I QT2 =D5TU-2.*TH1TU      I
      I QT1 =QT2*QT2      I
      I R1V6TU =2.4479922*QT1      I

```

```

      I

```

COMPUTE TUBE CONSTANT

```

      I
      I C9TU) =.10694444*D5TU/QT1      I

```

```

      I

```

SEE NEXT STATEMENT

```

      I
      I QT3 =C1HEAT*C9TU*F2MG*F2TEC*F2TCLN      I

```

```

I      /500.      I
      I

```

IF CONTRACT DESIGN FIND ORDERED TUBE LENGTH

```

      I
      I
      . * * .
    * * * * *
  I * * * * * I
  I * * * * * I
  I * * * * * I
- I * * * * * + I
-----
I 200 I      I 200 I      I 190 I
----+

```

```

      I
190      I XL1TUO =XL1TT-7.5      I
      I

```

COMPUTE EFFECTIVE TUBE LENGTH

```

      I
200      I XL1TUE =(XL1TUO-XL1TUI/6.)*XN2PS      I
      I

```

COMPUTE CIRC. WATER OUTLET TEMP.

```

      I
      I TE1O =TE1SAT-(TE1SAT-TE1INJ)/EXP(XL1TUE
      I      *QT3/SQRT(V1WTU))      I

```

COMPUTE CIRC. WATER TEMP. RISE

```
      I
      I TE1R =TE10-TE1INJ      I
      I
```

COMPUTE TERMINAL TEMP. DIFF.

```
      I
      I TE1TD=TE1SAT-TE10      I
      I
```

STOP PROGRAM IF TERMINAL TEMP. DIFF. LESS THAN 5 DEGREE

```
      I
      I
      . * * * .
      * (TE1TD.GE.5.) *
ON I I OFF
  I I
-----**
I GOTO102 I I
-----**
```

***WRITE(6,27)

```
      I
      I XL1TT=-1.      I
      I R9SW2=0.      I
      I S2TU =0.      I
      I XN2TUT =0.      I
      I A1TUSH =0.      I
      I D5TUSH =0.      I
```

```
I XL1CON =0. I
I W2COND =0. I
I VL1HW=0. I
```

```
I
I
--
I 300 I
--
```

COMPUTE CIRC. WATER REQ

```
I
202 I R9SW2=R9SF5*HT1SR/(500.*TE1R) I
I
```

COMPUTE TUBE SURFACE

```
I
I S2TU =XL1TUE*R9SW2*C9TU/V1WTU I
I
```

COMPUTE NUMBER OF TUBES

```
I
I L = (R9SW2*XN2PS/(R1V6TU*V1WTU)) I
I +1. I
I XN2TIT =L I
I
```


COMPUTE TUBE SHEET AREA

```

I
I QT1 =D5TU*D5TU*XN2TUT/(F2TUHO I
I *144.) I
I ALTUSH =.7854*QT1 I
I

```

COMPUTE TUBE SHEET DIAMETER

```

I
I D5T'JSH =SQRT(QT1) I
I

```

COMPUTE OVERALL LENGTH

```

I
I
I * * * * *
I * * * * * IF * *
I * * * * * (D5TUSH-7.5) * *
I * * * * * * * I
I * * * * * * * I
I * * * * * * * I
- I * * * * * * * + I
---*
I 215 I I 215 I I 210 I
---+-

```

```

I
210 I XL1CON =XL1TU0+7.5 I

```

```

I
I
--
I 220 I
--

```

```
                I
215      I XL1CON =XL1TUO+D5TUSH                I
```

```
                I
                I
                I
220      . * * *
      . * * * IF * *
    * * * * (XL1TT) * *
  I * * * * * * * I
  I * * * * * * * I
  I * * * * * * * I
- I * * * * * * * + I
-----
I 350 I      I 300 I      I 221 I
-----
```

```
                I
                I
                I
221      . * * *
      . * * * IF * *
    * * * * (XL1CON-XL1TT) * *
  I * * * * * * * I
  I * * * * * * * I
  I * * * * * * * I
- I * * * * * * * + I
-----
I 222 I      I 222 I      I 350 I
-----
```

```
                I
222      I MPTS =0                                I
                I
```

STORE OUTPUT VALUES

```
                I
300      I MPTS =MPTS+1                            I
```

```
                I
SEE NEXT STATEMENT                                QP1
```

```
                I
      I GP1(MPTS) =XL1TUO                            I
```

```
                I
SEE NEXT STATEMENT                                QP2
```

| | | |
|---------------------|---|-----|
| I | | |
| I QP2(MPTS) =S2TU | I | |
| I | | |
| SEE NEXT STATEMENT | | QP3 |
| I | | |
| I QP3(MPTS) =XL1TUE | I | |
| I | | |
| SEE NEXT STATEMENT | | QP4 |
| I | | |
| I QP4(MPTS) =XN2TUT | I | |
| I | | |
| SEE NEXT STATEMENT | | QP5 |
| I | | |
| I QP5(MPTS) =D5TUSH | I | |
| I | | |
| SEE NEXT STATEMENT | | QP6 |
| I | | |
| I QP6(MPTS) =A1TUSH | I | |
| I | | |
| SEE NEXT STATEMENT | | QP7 |
| I | | |
| I QP7(MPTS) =XL1CON | I | |
| I | | |
| SEE NEXT STATEMENT | | QP8 |
| I | | |
| I QP8(MPTS) =R9SW2 | I | |
| I | | |
| SEE NEXT STATEMENT | | QP9 |
| I | | |
| I QP9(MPTS) =TE10 | I | |

I
SEE NEXT STATEMENT

QR10

I
I QP10(MPTS) =TE1TD

I

I
SEE NEXT STATEMENT

QP11

I
I QP11(MPTS) =TE1R

I
I
I
I * * *
I * IF *
I * (MPTS-10) *
I * * * * *
I * * * * *
I * * * * *
- I 0 I + I

I 309 I I 350 I I 350 I
---**

309

I
I
I
I * * *
I * IF *
I * (XL1TT) *
I * * * * *
I * * * * *
I * * * * *
- I 0 I + I

I 350 I I 310 I I 320 I
--- -

310

I
I XL1TUO =XL1TUO+.5

I
I
I
I * * *
I * IF *
I * (XL1TUO-QL1TUO) *
I * * * * *
I * * * * *
I * * * * *
- I 0 I + I

I 200 I I 200 I I 350 I

40

```

320      I
      . * * .
      . * IF * .
      * (XL1CON-XL1TT) *
      I * . * * I
      I * . * * I
      I * . * * I
      - I      0 I      + I
      ----
      I 321 I      I 350 I      I 350 I
      ----

```

```

I
321      I XL1TUO =XL1TUO+.5      I
      I
      I
      --
      I 200 I
      --

```

PRINT OUTPUT

```

350      ***WRITE(6,40)(QP1(K),K=1,MPTS)
      ***WRITE(6,41)(QP2(K),K=1,MPTS)
      ***WRITE(6,42)(QP3(K),K=1,MPTS)
      ***WRITE(6,43)(QP4(K),K=1,MPTS)
      ***WRITE(6,44)(QP5(K),K=1,MPTS)
      ***WRITE(6,45)(QP6(K),K=1,MPTS)
      ***WRITE(6,46)(QP7(K),K=1,MPTS)
      ***WRITE(6,47)(QP8(K),K=1,MPTS)
      ***WRITE(6,48)(QP9(K),K=1,MPTS)
      ***WRITE(6,49)(QP10(K),K=1,MPTS)
      ***WRITE(6,50)(QP11(K),K=1,MPTS)
      I
      I
      . * * .
      . * IF * .
      * (XL1TT) *
      41

```

```

      . I * .
      I   * .
      I     * . *
      - I       0 I       + I
      ---
      I 1000I      I 400 I      I 500 I
      -----

```

PLOT DIAMETER VERSUS LENGTH

```

      I
400      I QT1 =QP5(1)      I
      I QT2 =QP5(1)      I

      I
      SEE NEXT STATEMENT      QLL

      I
      I QLL =QP7(1)      I

      I
      SEE NEXT STATEMENT      QLR

      I
      I QLR =QP7(1)      I

      I
      I
      + DO      +
      + DO      +
      + K=2,MPTS      +
      +      +
      I
      I
      I QT1 =AMIN1(QT1,QP5(K))      I
      I QT2 =AMAX1(QT2,QP5(K))      I
      I QLL =AMIN1(QLL,QP7(K))      I
      I
      I
410 +++++++I QLR =AMAX1(QLR,QP7(K))      I

      I
      SEE NEXT STATEMENT      QDX

```

```

SEE NEXT STATEMENT                                MERR

      CALL DXDYV (1,QLL,QLR,QDX,N,I,NX,20.,MERR)

SEE NEXT STATEMENT                                QDY

      CALL DXDYV (2,QT1,QT2,QDY,M,J,NY,20.,MERR)
      CALL GRID1V (3,QLL,QLR,QT1,QT2,QDX,QDY,N,M,-I,-J,NX,NY)
      CALL PRINTV (-11,11HLENGTH FT.,492,4)
      CALL PRINTV (72,QTITLE,244,1012)
      CALL APRNTV (0,-14,-13,13HDIAMETER FT.,4,584)

```

```

SEE NEXT STATEMENT                                MX1

```

```

      I
      I MX1 =NXV(QP7(1))                            I

```

```

      I
SEE NEXT STATEMENT                                MY1

```

```

      I
      I MY1 =NYV(QP5(1))                            I

```

```

      I
      I
      + DO
+++++++ 420
      + K=2,MPTS
      +

```

```

+ SEE NEXT STATEMENT                                MX2

```

```

+      I
+      I MX2 =NXV(QP7(K))                            I

```

```

+ SEE NEXT STATEMENT                                MY2

```

```

+      I
+      I MY2 =NYV(QP5(K))                            I

```

```

+      I
+ CALL LINEV (MX1,MY1,MX2,MY2)
+      I

```

```

+
+      I MX1  =MX2      I
+
+      I
+
+
420 ++++++I MY1  =MY2      I
      I
      I
      --
      I 1000I
      --

```

CHECK CONDENSER WIDTH

```

500
      I
      I
      . * * *
      . * * * IF * *
      * (D5COND-QP5(1)) *
      I . * * * * I
      I * * * * * I
      I * * * * * I
      - I      0 I      + I
      ----
      I 501 I      I 510 I      I 510 I
      -- *

```

```

501      ***WRITE'6,28)
      I
      --
      I 1000I
      --

```

PLOT HEAT LOAD VERSUS ABSOLUTE PRESSURE

```

      I
510      I QT1  =R9SF5*HT1SR      I
      I QT2  =QT1/50.      I
      I QLL  =QT1*.1      I

```


I QT1 =QLL+QT1

I

I

CALL GRID1V (3,QLL,QT1,10.,0.,QT2,.2,5,5,-10,-5,-6,2)

CALL PRINTV (72,QTITLE,244,1020)

CALL PRINTV (-17,17HHEAT LOAD BTU/HR,460,4)

CALL APKNIV (0,-14,-24,24HABSOLUTE PRESSURE IN HG,4,656)

CALL PRINTV (-19,19HCIRC WATER VELOCITY,816,1006)

CALL PRINTV (-17,17HIN TUBES (FT/SEC),824,990)

SEE NEXT STATEMENT

QTC

I

I QTC =647.27

I

I

SEE NEXT STATEMENT

QPC

I

I QPC =6527.90844

I

I MPTS =11

I

I MX1 =V1WTU

I

I V1WTU=MX1

I

I

520

I QT1 =EXP(QT3*XL1TUE/SQRT(V1WTU))

I

I R9SW2=XN2TUT*R1V6TU*V1WTU/XN2PS

I

I QT2 =0.

I

I

I

+

+

+ DO

+

+++++

550

+

+ I=1,MPTS

+

+

+

+

I

I

+

I QT2 =QT2+QLL

I

+

I QP1(I) =QT2

I

+

I TE10 =TE1INJ+QT2/(500.*R9SW2)

I

+

I TE1SAT =(QT1*TE10-TE1INJ)/(QT1

I

+

I -1.)

I

+

I

I

I

+

. * * IF * .

```

+      * (TE1SAT-200.) *
+      I * . * . * . * I
+      I * . * . * . * I
+      I * . * . * . * I
+      - I      0 I      + I
+      -- -
+ I 530 I      I 531 I      I 531 I
+ ---*+
+
+      I
+
+      I L      =1
530 +      I
+      I
+      --
+      I 535 I
+      -*
+
+      I
+
+      I L      =2
531 +      I
+      I
+
+      I TE1SAT =(TE1SAT-32.)*5./9.+273.16
535 +      I QDX =QTC-TE1SAT
+      I QDY =QDX/TE1SAT*(((QPFT(3,L)+QPFT(5,L)
+      I      *QDX)*QDX*QDX+
+      I      QPFT(2,L))*QDX+QPFT(1,L))/(1.+QPFT(4,L)*QDX)
+      I P2BDES =QPC/10.**QDY
+      I
+      I
+
+      I
550 ++++++I QP2(I) =P2BDES
+      I MX1 =NXV(QP1(1))
+      I MY1 =NYV(QP2(1))
+      I
+      I
+      I
+      +
+      + DO
+++++*+      +
+      + 560
+      + K=2,MPTS
+      +
+      I
+      I
+
+      I MX2 =NXV(QP1(K))
+      I
+      I
+      I
+      . * * . * .
+      . * * IF * .
+      * (QP2(K)-10.) *
+      I * . * . * . * I
+      I * . * . * . * I

```

```

+   I           * . *           I
+  - I           0 I           + I
+
+ I 555 I       I 555 I       I 561 I
+
+           I
+
555 +       I MY2 =NYV(QP2(K))           I
+
+           I
+       CALL LINEV (MX1,MY1,MX2,MY2)
+           I
+       I MX1 =MX2           I
+
+           I
560 ++++++I MY1 =MY2           I
+
+           I
561       I MY1 =MY1+3           I
+
+           I
+       CALL LABLV (V1WTU,MX1,MY1,3,1,3)
+           I
+       I MX1 =MX1+24           I
+
+           I
+       CALL PRINTV (-4,4H FPS,MX1,MY1)
+           I
+       I V1WTU=V1WTU-1.           I
+
+           I
+           I
+           I
+           . * . * . * .
+           . * . * . * .
+           * . * . * . * .
+       I * . * . * . * . * I
+       I * . * . * . * . * I
+       I * . * . * . * . * I
+       - I           0 I           + I
+
+ I 1000I       I 520 I       I 520 I
+
1000       CALL FVEFN (1,16)
+
+       CALL MZEFN (1,1)
+
+       STOP
END
*       *

```

B. Program Listing

C I. IDENTIFICATION
 C A. TITLE - STEAM CONDENSER DESIGN
 C 1. FORTRAN IV DECKNAME - COND
 C 2. REVISION - A - ORIGINAL ISSUE
 C B. ABSTRACT - THIS PROGRAM CALCULATES ALL THE NECESSARY
 C INFORMATION REQUIRED FOR THE SELECTION OF MAIN OR AUXILIARY
 C STEAM CONDENSERS TO EITHER PRELIMINARY OR CONTRACT DESIGN
 C REQUIREMENTS.
 C FOR PRELIMINARY DESIGN A GRAPH IS ALSO PROVIDED WHICH
 C RELATES CONDENSER OVERALL LENGTH WITH TUBE SHEET DIAMETER
 C FOR A SPECIFIED SET OF DESIGN CONDITIONS. FOR CONTRACT
 C DESIGN A GRAPH RELATING CONDENSER ABSOLUTE PRESSURE AND
 C INCREMENTS OF HEAT REJECTION AT INTEGER CIRCULATING WATER
 C VELOCITIES IS ALSO PROVIDED FOR ANALYSIS OF PART LOAD
 C PERFORMANCE.
 C C. INPUT / CALCULATED ITEMS / OUTPUT
 C 1. INPUT

| | |
|--|--------|
| TUBE MATERIAL | XMA1TU |
| TUBE GAGE | GA1TU |
| TUBE OUTSIDE DIAMETER (INCHES) | D5TU |
| NUMBER OF PASSES | XN2PS |
| CLEANLINESS FACTOR | F2TCLN |
| NUMBER OF TUBE SHEETS PER END | XN2TSE |
| INEFFECTIVE TUBE LENGTH PER END (INCHES) | XL1TUI |
| TUBE HOLE SPACE FACTOR | F2TUHO |
| STEAM FLOW TO CONDENSER (LB/HR) | R9SF5 |
| HEAT REJECTED PER POUND OF STEAM (BTU/LB) | HT1SR |
| DESIGN BACK PRESSURE (INCHES - HG) | P2BDES |
| INJECTION WATER TEMPERATURE (DEG F) | TE1INJ |
| OVERALL CONDENSER LENGTH (FT) | XL1TT |
| DESIRED DIAMETER OF TUBE SHEET (FT) | D5COND |
| CIRCULATING WATER VELOCITY IN TUBES (FT/SEC) | V1WTU |
| ORDERED TUBE LENGTH SHORTEST | XL1TUO |
| ORDERED TUBF LENGTH LONGEST | QL1TUO |

C 2. INTERNAL VALUES

| | |
|---------------------------------|--------|
| TUBE WALL THICKNESS | TH1TU |
| BASIC HEAT TRANSFER COEFFICIENT | C1HEAT |
| TUBE CONSTANT | C9TU |
| MATERIAL AND GAGE FACTOR | F2MG |
| TEMPERATURE CORRECTION FACTOR | F2TEC |
| GPM / 1 FPS / TUBE | R1V6TU |

C 3. OUTPUT

| | |
|------------------------------------|--------|
| TEMPERATURE SATURATED LIQUID | TE1SAT |
| ORDERER TUBE LENGTH | XL1TUO |
| TUBE SURFACE AREA | S2TU |
| EFFECTIVE TUBE LENGTH | XL1TUE |
| NUMBER OF TUBES | XN2TUT |
| TUBE SHEET DIAMETER | D5TUSH |
| TUBE SHEET AREA | ALTUSH |
| OVERALL CONDENSER LENGTH | XL1CON |
| CIRCULATING WATER REQUIRED (GPM) | R9SW2 |
| CIRCULATING WATER OUTLET TEMP. | TE1O |
| TERMINAL TEMPERATURE DIFF. | TE1TD |
| CIRCULATING WATER TEMPERATURE RISE | TE1R |

C D. AUTHOR/DATE
 C MAXINE BOTTING DENIS KELLY DECEMBER 1965
 C E. ORGANIZATION
 C COMPUTER-AIDED SHIP DESIGN DIVISION, CODE 850,
 C DAVID TAYLOR MODEL BASIN
 C F. COMPUTER/SOURCE LANGUAGE

```

C      - IBM 7090      FORTRAN IV
C      G. REFERENCE TO DOCUMENTATION
C      DTMB REPORT 2255 OF JULY 1966
C      H. SECURITY CLASSIFIED
C      UNCLASSIFIED
C      I. ESTIMATED RUNNING TIME
C      1 1/2 MINUTES
COMMON XMA1TU,GAI1TU,D5TU,F2TCLN,XN2TSE,XL1TUI
COMMON F2TUHO,XN2PS,R9SF5,HT1SR,P2BDES,V1WTU
COMMON TE1INJ,XL1TT,D5COND,XL1TUO,QL1TUO
COMMON S2TU,XL1TUE,XN2TUT,D5TUSH,A1TUSH,XL1CON
COMMON R9SW2,TE1O,TE1TD,TE1R,W2COND,VL1HW
DIMENSION QTITLE(12)
DIMENSION QMA(2)
DIMENSION QAA(9),QCU(7,2),QCF(15),QTH(7)
DIMENSION QPFT(5,2)
DIMENSION QP1(11),QP2(11),QP3(10),QP4(10),QP5(10),QP6(10),QP7(10),
1QP8(10),QP9(10),QP10(10),QP11(10) 456 BYTES
C      SEE DATA STATEMENT                                QAA
C      SEE DATA STATEMENT                                QCU
C      SEE DATA STATEMENT                                QCF
C      SEE DATA STATEMENT                                QTH
C      SEE DATA STATEMENT                                QPFT
DATA QAA/35.15789,24.592588,2.1182069,-.3414474,.15741642,
1-.3132958E-1,.38658282E-2,-.24901784E-3,.68401559E-5/
DATA QCU/.46,.55,.64,.71,.76,.80,.83,.55,.64,.72,.79,.84,
1.87,.90/
DATA QCF/.65,.7,.75,.798,.843,.886,.926,.963,1.,1.025,
11.045,1.061,1.076,1.09,1.1/
DATA QTH/.109,.095,.083,.072,.065,.058,.049/
DATA QPFT/3.2437814,.00586826,1.1702379E-8,.0021878462,0.,
13.346313,.0414113,7.515484E-9,.013794481,6.56444E-11/
DATA QMA/6H 70-30,6H 90-10/
1 FORMAT (12A6)
2 FORMAT (1H1,/,24X,12A6,/,13H0INPUT VALUES,/)
3 FORMAT (6E12.6)
5 FORMAT (14H0TUBE MATERIAL,40X,A6 /10H TUBE GAGE,30X,F20.0,/20H
1TUBE DIAMETER (IN),20X,F20.4)
6 FORMAT (19H CLEANLINESS FACTOR,21X,F20.4,/30H NUMBER OF TUBE SHEET
1S PER END,10X,F20.0,/38H INEFFECTIVE TUBE LENGTH PER END (IN),F22
2.4)
7 FORMAT (23H TUBE HOLE SPACE FACTOR,17X,F20.4,/17H NUMBER OF PASSES
1,23X,F20.0,/28H STEAM TO CONDENSER (LB/HR),F32.0)
8 FORMAT (43H HEAT REJECTED PER POUND OF STEAM (BTU/LB),F17.2,/30H
1DESIGN BACK PRESSURE (IN HG),F30.2 ,/39H CIRC WATER VELOCITY IN T
2UBES (FT/SEC),F21.2)
9 FORMAT (37H INJECTION WATER TEMPERATURE (DEG F),F23.2,/39H DESIRE
1D OVERALL CONDENSER LENGTH (FT),F21.2,/37H DESIRED DIAMETER OF TU
2BE SHEET (FT),F23.2)
10 FORMAT (36H ORDERED TUBE LENGTH SHORTEST (FT),F24.2,/35H ORDERED
1 TUBE LENGTH LONGEST (FT),F25.2)
15 FORMAT (6E20.8)
20 FORMAT (22H0INPUT VALUE P2BDES IS,E15.8,5X,28HSHOULD BE BETWEEN .2
1 AND 450)
21 FORMAT (22H0INPUT VALUE TE1INJ IS,E15.8,5X,28HSHOULD BE BETWEEN 30
1 AND 100)
22 FORMAT (21H0INPUT VALUE GAI1TU IS,E15.8,5X,27HSHOULD BE BETWEEN 12
1AND 18)
23 FORMAT (22H0INPUT VALUE XMA1TU IS,E15.8,5X,16HSHOULD BE 1 OR 2)
24 FORMAT (19H0XL1TUI IS NEGATIVE,E15.8)

```

```

25 FORMAT (22H0INPUT VALUE XN2TSE IS,E15.8,5X,16HSHOULD BE 1 OR 2)
26 FORMAT (19H0F2TUHO IS NEGATIVE,E15.8)
27 FORMAT (1H0,30X,36HTERMINAL TEMP DIFF LESS THAN 5 DEG F)
28 FORMAT (36H0DIAMETER OF TUBE SHEET IS TOO LARGE)
39 FORMAT (14H1OUTPUT VALUES, //38HOTEMPERATURE SATURATED LIQUID (DEG
1 F),F22.4)
40 FORMAT (26H0ORDERED TUBE LENGTH (FT),4X,10F9.2)
41 FORMAT (27HOTUBE SURFACE AREA (SQ FT),3X,10F9.0)
42 FORMAT (28H0EFFECTIVE TUBE LENGTH (FT),2X,10F9.2)
43 FORMAT (16H0NUMBER OF TUBES,14X,10F9.0)
44 FORMAT (26HOTUBE SHEET DIAMETER (FT),4X,10F9.2)
45 FORMAT (25HOTUBE SHEET AREA (SQ FT),5X,10F9.2)
46 FORMAT (31H0OVERALL CONDENSER LENGTH (FT),F8.2,9F9.2)
47 FORMAT (30H0CIRCULATING WATER REQD (GPM),10F9.0)
48 FORMAT (32H0CIRC WATER OUTLET TEMP (DEG F),F7.2,9F9.2)
49 FORMAT (28HOTERMINAL TEMP DIFF (DEG F),2X,10F9.2)
50 FORMAT (30H0CIRC WATER TEMP RISE (DEG F),10F9.2)
CALL CAMRAV (35)

```

```

C
C READ INPUT
C
C SEE NEXT STATEMENT QTITLE
C READ(5,1)QTITLE
C READ(5,3)XMA1TU,GA1TU,D5TU,F2TCLN,XN2TSE,XL1TUI
C READ(5,3)F2TUHO,XN2PS,R9SF5,HT1SR,P2BDES,V1WTU
C SEE NEXT STATEMENT QL1TUO
C READ(5,3)TE1INJ,XL1TT,D5COND,XL1TUO,QL1TUO
C
C PRINT INPUT
C
C WRITE(6,2)QTITLE
C I=XMA1TU
C WRITE(6,5)QMA(I),GA1TU,D5TU
C WRITE(6,6)F2TCLN,XN2TSE,XL1TUI
C WRITE(6,7)F2TUHO,XN2PS,R9SF5
C WRITE(6,8)HT1SR,P2BDES,V1WTU
C WRITE(6,9)TE1INJ,XL1TT,D5COND
C WRITE(6,10)XL1TUO,QL1TUO
C SEE NEXT STATEMENT MPTS
C MPTS=0
C P2BDES=P2BDES*.49115
C
C COMPUTE TEMPERATURE OF SATURATED LIQUID
C
C IF(P2BDES-.2) 105,106,106
105 WRITE(6,20)P2BDES
C STOP
106 IF(P2BDES-450.) 109,105,105
109 TE1SAT=QAA(1)
C SEE NEXT STATEMENT QT1
C QT1=1.
C SEE NEXT STATEMENT QT2
C QT2=ALOG(10.*P2BDES)
C DO 110 K=2,9
C QT1=QT1*QT2
110 TE1SAT=TE1SAT+QAA(K)*QT1
C WRITE (6,39)TE1SAT
C
C COMPUTE CIRC WATER CORRECTION FACTOR
C
C

```

```

      IF(TE1INJ-30.) 115,116,116
115 WRITE(6,21)TE1INJ
      STOP
116 IF(TE1INJ-100.) 120,120,115
120 K=TE1INJ/5.-5.
      QT1=(K+5)*5
      F2TEC=QCF(K)+(QCF(K+1)-QCF(K))*(TE1INJ-QT1)*.2
C
C   FIND WALL THICKNESS
C
      IF(GA1TU-12.) 121,122,122
121 WRITE(6,22)GA1TU
      STOP
122 IF(GA1TU-18.) 125,125,121
125 K=GA1TU-11.
      TH1TU=QTH(K)
C
C   FIND MATERIAL FACTOR
C
      IF(XMA1TU-1.) 126,128,127
126 WRITE(6,23)XMA1TU
      STOP
127 IF(XMA1TU-2.) 126,128,126
128 L=XMA1TU
      F2MG=QCU(K,L)
C
C   COMPUTE INEFFECTIVE TUBE LENGTH PER END
C
      IF(XL1TUI) 140,145,150
140 WRITE(6,24)XL1TUI
      STOP
145 IF(XN2TSE-1.) 146,147,148
146 WRITE(6,25)XN2TSE
      STOP
147 XL1TUI=1.0625
      GO TO 150
148 IF(XN2TSE-2.) 146,149,146
149 XL1TUI=6.25
C
C   COMPUTE TUBE HOLE SPACE FACTOR
C
150 IF(F2TUHO) 151,152,160
151 WRITE(6,26)F2TUHO
      STOP
152 IF(P2BDES-1.25) 153,153,154
153 F2TUHO=.22
      GO TO 160
154 F2TUHO=.24
C
C   COMPUTE HEAT TRANSFER COEFFICIENT
C
160 IF(D5TU-.875) 162,161,161
161 C1HEAT=263.
      GO TO 180
162 C1HEAT=270.
C
C   COMPUTE GPM / TUBE / 1 FPS VELOCITY
C
180 QT2=D5TU-2.*TH1TU
      QT1=QT2*QT2

```

```

R1V6TU =2.4479922*QT1
C
C COMPUTE TUBE CONSTANT
C
C9TU=.10694444*D5TU/QT1
C SEE NEXT STATEMENT
C QT3=C1HEAT*C9TU*F2MG*F2TEC*F2TCLN/500.
C
C IF CONTRACT DESIGN FIND ORDERED TUBE LENGTH
C
C IF(XL1TT) 200,200,190
190 XL1TUO=XL1TT-7.5
C
C COMPUTE EFFECTIVE TUBE LENGTH
C
200 XL1TUE=(XL1TUO-XL1TUI/6.)*XN2PS
C
C COMPUTE CIRC. WATER OUTLET TEMP.
C
TE10=TE1SAT-(TE1SAT-TE1INJ)/EXP(XL1TUE*QT3/SQRT(V1WTU))
C
C COMPUTE CIRC. WATER TEMP. RISE
C
TE1R=TE10-TE1INJ
C
C COMPUTE TERMINAL TEMP. DIFF.
C
TE1TD=TE1SAT-TE10
C
C STOP PROGRAM IF TERMINAL TEMP. DIFF. LESS THAN 5 DEGREE
C
C IF(TE1TD.GE.5.) GO TO 202
WRITE(6,27)
XL1TT=-1.
R9SW2=0.
S2TU=0.
XN2TUT=0.
A1TUSH=0.
D5TUSH=0.
XL1CON=0.
W2COND=0.
VL1HW=0.
GO TO 300
C
C COMPUTE CIRC. WATER REQ T
C
202 R9SW2=R9SF5*HT1SR/(500.*TE1R)
C
C COMPUTE TUBE SURFACE
C
S2TU=XL1TUE*R9SW2*C9TU/V1WTU
C
C COMPUTE NUMBER OF TUBES
C
L=(R9SW2*XN2PS/(R1V6TU*V1WTU))+1.
XN2TUT=L
C
C COMPUTE TUBE SHEET AREA
C
QT1=D5TU*D5TU*XN2TUT/(F2TUHO*144.)

```



```

      A1TUSH=.7854*QT1
C
C   COMPUTE TUBE SHEET DIAMETER
C
      D5TUSH=SQRT(QT1)
C
C   COMPUTE OVERALL LENGTH
C
      IF(D5TUSH-7.5) 215,215,210
210  XL1CON=XL1TUO+7.5
      GO TO 220
215  XL1CON=XL1TUO+D5TUSH
220  IF(XL1TT) 350,300,221
221  IF(XL1CON-XL1TT) 222,222,350
222  MPTS=0
C
C   STORE OUTPUT VALUES
C
300  MPTS=MPTS+1
C   SEE NEXT STATEMENT
      QP1(MPTS)=XL1TUO
C   SEE NEXT STATEMENT
      QP2(MPTS)=S2TU
C   SEE NEXT STATEMENT
      QP3(MPTS)=XL1TUE
C   SEE NEXT STATEMENT
      QP4(MPTS)=XN2TUT
C   SEE NEXT STATEMENT
      QP5(MPTS)=D5TUSH
C   SEE NEXT STATEMENT
      QP6(MPTS)=A1TUSH
C   SEE NEXT STATEMENT
      QP7(MPTS)=XL1CON
C   SEE NEXT STATEMENT
      QP8(MPTS)=R9SW2
C   SEE NEXT STATEMENT
      QP9(MPTS)=TE1O
C   SEE NEXT STATEMENT
      QP10(MPTS)=TE1TD
C   SEE NEXT STATEMENT
      QP11(MPTS)=TE1R
      IF(MPTS-10) 309,350,350
309  IF(XL1TT) 350,310,320
310  XL1TUO=XL1TUO+.5
      IF(XL1TUO-QL1TUO) 200,200,350
320  IF(XL1CON-XL1TT) 221,350,350
321  XL1TUO=XL1TUO+.5
      GO TO 200
C
C   PRINT OUTPUT
C
350  WRITE(6,40)(QP1(K),K=1,MPTS)
      WRITE(6,41)(QP2(K),K=1,MPTS)
      WRITE(6,42)(QP3(K),K=1,MPTS)
      WRITE(6,43)(QP4(K),K=1,MPTS)
      WRITE(6,44)(QP5(K),K=1,MPTS)
      WRITE(6,45)(QP6(K),K=1,MPTS)
      WRITE(6,46)(QP7(K),K=1,MPTS)
      WRITE(6,47)(QP8(K),K=1,MPTS)
      WRITE(6,48)(QP9(K),K=1,MPTS)

```

```

WRITE(6,49)(QP10(K),K=1,MPTS)
WRITE(6,50)(QP11(K),K=1,MPTS)
IF(XL1TT) 1000,400,500
C
C   PLOT DIAMETER VERSUS LENGTH
C
400 QT1=QP5(1)
    QT2=QP5(1)
C   SEE NEXT STATEMENT
    QLL=QP7(1)
C   SEE NEXT STATEMENT
    QLR=QP7(1)
    DO 410 K=2,MPTS
    QT1=AMIN1(QT1,QP5(K))
    QT2=AMAX1(QT2,QP5(K))
    QLL=AMIN1(QLL,QP7(K))
410 QLR=AMAX1(QLR,QP7(K))
C   SEE NEXT STATEMENT
C   SEE NEXT STATEMENT
    CALL DXDYV (1,QLL,QLR,QDX,N,I,NX,20.,MERR)
C   SEE NEXT STATEMENT
    CALL DXDYV (2,QT1,QT2,QDY,M,J,NY,20.,MERR)
    CALL GRID1V (3,QLL,QLR,QT1,QT2,QDX,QDY,N,M,-I,-J,NX,NY)
    CALL PRINTV (-11,11HLENGTH FT.,492,4)
    CALL PRINTV (72,QTITLE,244,1012)
    CALL APRNTV (0,-14,-13,13HDIAMETER FT.,4,584)
C   SEE NEXT STATEMENT
    MX1=NXV(QP7(1))
C   SEE NEXT STATEMENT
    MY1=NYV(QP5(1))
    DO 420 K=2,MPTS
C   SEE NEXT STATEMENT
    MX2=NXV(QP7(K))
C   SEE NEXT STATEMENT
    MY2=NYV(QP5(K))
    CALL LINEV (MX1,MY1,MX2,MY2)
    MX1=MX2
420 MY1=MY2
    GO TO 1000
C
C   CHECK CONDENSER WIDTH
C
500 IF(D5COND-QP5(1)) 501,510,510
501 WRITE(6,28)
    GO TO 1000
C
C   PLOT HEAT LOAD VERSUS ABSOLUTE PRESSURE
C
510 QT1=R9SF5*HT1SR
    QT2=QT1/50.
    QLL=QT1*.1
    QF1=QLL+QT1
    CALL GRID1V (3,QLL,QT1,10.,0.,QT2,.2,5,5,-10,-5,-6,2)
    CALL PRINTV (72,QTITLE,244,1020)
    CALL PRINTV (-17,17HHEAT LOAD BTU/HR,460,4)
    CALL APRNTV (0,-14,-24,24HABSOLUTE PRESSURE IN HG,4,656)
    CALL PRINTV (-19,19HCIRC WATER VELOCITY,816,1006)
    CALL PRINTV (-17,17HIN TUBES (FT/SEC),824,990)
C   SEE NEXT STATEMENT
    QTC=647.27

```

```

C      SEE NEXT STATEMENT
      QPC=6527.90844
      MPTS=11
      MX1=V1WTU
      V1WTU=MX1
520  QT1=EXP(QT3*XL1TUE/SQRT(V1WTU))
      R9SW2=XN2TUT*R1V6TU*V1WTU/XN2PS
      QT2=0.
      DO 550 I=1,MPTS
      QT2=QT2+QLL
      QP1(I)=QT2
      TE10=TE1INJ+QT2/(500.*R9SW2)
      TE1SAT=(QT1*TE10-TE1INJ)/(QT1-1.)
      IF(TE1SAT-200.) 530,531,531
530  L=1
      GO TO, 535
531  L=2
535  TE1SAT=(TE1SAT-32.)*5./9.+273.16
      QDX=QTC-TE1SAT
      QDY=QDX/TE1SAT*(((QPFT(3,L)+QPFT(5,L)*QDX)*QDX*QDX+
1QPFT(2,L))*QDX+QPFT(1,L))/(1.+QPFT(4,L)*QDX)
      P2BDES=QPC/10.**QDY
550  QP2(I)=P2BDES
      MX1=NXV(QP1(I))
      MY1=NYV(QP2(I))
      DO 560 K=2,MPTS
      MX2=NXV(QP1(K))
      IF(QP2(K)-10.) 555,555,561
555  MY2=NYV(QP2(K))
      CALL LINEV (MX1,MY1,MX2,MY2)
      MX1=MX2
560  MY1=MY2
561  MY1=MY1+3
      CALL LABLV (V1WTU,MX1,MY1,3,1,3)
      MX1=MX1+24
      CALL PRINTV (-4,4H FPS,MX1,MY1)
      V1WTU=V1WTU-1.
      IF(V1WTU-3.) 1000,520,520
1000 CALL FVEFN (1,16)
      CALL MZEFN(1,1)
      STOP
      END

```

QPC

C. Special Diagnostics

(1) Design Back Pressure

Input value P2BDES is _____

should be between .2 and 450

Program stopped.

(2) Injection water Temperature.

Input value TEIINJ is _____

Should be between 30 and 100

Program is stopped.

(3) Tube Gage

Input value GAITU is _____

Should be between 12 and 18

Program is stopped.

(4) Effective Tube Length

XL1TUE is negative

Program is stopped.

(5) Number of Tube Sheets per end

Input value XN2TSE is _____

Should be 1 or 2

Program is stopped.

(6) Tube Material

Input value XMA1TU is _____

Should be 1 or 2

Program is stopped.

(7) Tube Hole Space Factor

F2TUHO is negative •

Program is stopped.

VII. ACKNOWLEDGMENT

This program utilizes coefficients derived by Raymond W. Yaw,
Code 6436, NAVSEC.

REFERENCES

- 1. Design Data Sheet DDS4601-1 of 15 October 1953 - Steam Condensers.**
- 2. Military Specification MIL-C-15430G Condensers, Steam Surface, Naval Shipboard.**
- 3. Share Programs C3-WH58-PA-3137 (Westinghouse Corporation Properties of Steam).**

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